Deep eutectic solvents (DESs) are noted to be green ionic liquid (IL) analogues, and their many favourable properties made them interesting for the scientific community. In this study, two novel DESs of citric acid with the monosaccharides D-glucose or D-fructose (1:1 molar ratio) were prepared and characterized. At the atmospheric pressure, the density, the dynamic viscosity, and the electrical conductivity of these eutectic solvents were measured and analysed as the function of temperature in the practical temperature range of 293.15-363.15 K. Arrhenius theory was employed for understanding the transport phenomena in these DESs. By using the experimental data, some important properties were calculated such as molecular volume, lattice energy, heat capacity, molar Gibbs energy, enthalpy and entropy of activation of viscous flow for the synthesized DESs. The fractional Walden rule was employed to establish the relationship between molar conductivity and viscosity, which proved an excellent linear behaviour.

Finally, these DESs were tested as cosolvents in oleic acid (oA) ethanolysis. The investigated DESs possess many desirable properties, such as low vapour pressure, inflammability, biodegradability, and can be obtained from available renewable resources. These DESs showed to have the potential to be utilized for several industrial applications, like processing and separation of food constituents, pharmaceutical applications, and mediums for chemical reactions.
determined at several temperatures. Correlations for the temperature dependences of the measured properties are done and discussed in the terms of Arrhenius theory.

The fractional Walden rule was used to study the relationship between the molar conductivity and the viscosity. At last, the possibilities of using these DESs as cosolvents in OA ethanolysis were reflected.

**Experimental**

**Materials**

Citric acid monohydrate (99.5%) was purchased from Zorka Šabac, Serbia. D-glucose (99.0%) and D-fructose (99.0%) were obtained from MosLab Belgrade, Serbia. Oleic acid and concentrated sulphuric acid (reagent grade 98.0%) were provided from Sigma-Aldrich. Absolute ethanol (99.5%) was purchased from Lachema (Czech Republic). Also, the following solvents were used: n-hexane (99.0%, Promochem, Germany), n-hexane and 2-propanol (HPLC grade, JT Baker). The standard for ethyl oleate was purchased from Sigma Co. All reagents were used without further purification.

**Preparation of DESs**

To prepare the DESs, citric acid was mixed with D-glucose or D-fructose at 1:1 molar ratio in a round-bottomed flask. The flask was then placed on a rotary evaporator, at 348.15 K until a homogeneous liquid was formed. DESs were stored in well-closed, glass bottles in a desiccator containing CaCl₂. Figure 1 represents DESs preparation process, and visible properties of the prepared DESs at room temperature are listed in Table 1.

![Figure 1. Preparation of deep eutectic solvents](image)

**Table 1. Prepared DESs and their visible properties at room temperature**

<table>
<thead>
<tr>
<th>DES</th>
<th>Composition</th>
<th>Citric acid: monosaccharide molar ratio (mol/mol)</th>
<th>Visible properties of DES at room temperature</th>
</tr>
</thead>
<tbody>
<tr>
<td>DES1</td>
<td>Citric acid:D-glucose</td>
<td>1:1</td>
<td>Liquid, viscous, homogeneous, light yellow</td>
</tr>
<tr>
<td>DES2</td>
<td>Citric acid:D-fructose</td>
<td>1:1</td>
<td>Liquid, viscous, homogeneous, dark brown</td>
</tr>
</tbody>
</table>

**Measurements of the physical properties of DESs**

Physical properties (density, dynamic viscosity, and electrical conductivity were measured for synthesized DESs within 293.15-363.15 K temperature range. All measurements were performed three times at each temperature, in the air at ambient pressure, and their mean values were used for comparison. The dependences of the selected physical property with temperature were established for each system and the corresponding “best” equations for the same temperature range were conducted. The temperature dependent equations were systematized for each property. Karl-Fischer moisture titrator (Metrohm 73KF coulometer) was used to determine the water content of the dried DESs, and the values were less than 300 ppm.

**Measurements of the densities of DESs**

At atmospheric pressure, the densities (ρ) of all samples of DESs were measured with a DMA 4500 Anton Paar densitometer. The sample thermostating was controlled to ± 0.1 K.
Oleic acid ethanolysis

Figure 2 shows the reaction of OA ethanolysis and the reaction conditions of the OA ethanolysis applied are provided in Table 2. The apparatus for the reaction consisted of a 250 mL two-neck round-bottomed flask, placed in a glass chamber, equipped with a magnetic stirrer and a condenser. Water was circulated through the chamber from a thermostated bath. In the first series of experiments, where the effect of DESs was studied, the predetermined amounts of selected DES (4.60 g) and ethanol (14.38 g) were added into the flask. Sulfuric acid (0.23 g) was added to the mixture drop by drop. Oleic acid (22.98 g) was preheated in a glass beaker and then added into the flask. The mixture in the flask was stirred magnetically at 500 rpm for 6 h at 70 °C. In the second series of experiments, DES was not added, and in the third series only DESs were used, without sulfuric acid. During the reaction, at various time intervals, the samples were taken from the reaction mixture (1 cm³). After the reaction, the reaction mixture was poured into a conical shaped separatory funnel and allowed to settle. All experiments were run in duplicate. The samples were centrifuged for 15 min at 3500 min⁻¹. The upper layer consists of ethyl oleate and oleic acid, and the bottom layer is a mixture of sulfuric acid, water and selected DES. The quantitative composition of the upper layer (dilution 1:200 in a mixture of 2-propanol/n-hexane; 5:4 v/v) was determined by liquid chromatography (HPLC).

Analytical methods

The samples (1 mL) were removed from the reaction mixture during the progress of the ethanolysis reaction, cooled in an ice bath, and centrifuged (3500 rpm, 10 min). The upper layer (named ester fraction) was withdrawn, dissolved in 2-propanol/n-hexane (5:4 v/v) in an appropriate ratio, and filtered through a 0.45 μm Millipore filter. The resulting filtrate was used for a high performance liquid chromatography (HPLC) analysis, which was described in details by Stamenković et al. [21]. The conversion degree of OA (XA) was calculated from the content of OA (in %) in the ester/oil fraction of the reaction mixture, by the following equation (1):

$$X_A = \frac{(100 - OA_{\text{final}})}{100}$$

where OA_{final} is the percentage of OA in the ester/oil fraction.

Results And Discussions

The effect of temperature on the physical properties of two citric acid-based deep eutectic solvents

The effect of temperature on the density of two citric acid-based deep eutectic solvents

Density represents a very important property of chemical materials. In order to obtain the data needed for a technological design, the knowledge of the temperature effect on density is very significant for engineers. Also, the thermal expansion coefficient or compressibility coefficients obtained from density can provide a liquid structure and interactions data. If the temperature of the system rises, the molecules are moving at higher speeds, so the molar volume of the solution increases. The result of this is density reduction.
\[ \rho = a + b \cdot T \]  

where the parameters “a” (the density at 0 K in kg·m\(^{-3}\)) and “b” (the coefficient of volume expansion in kg·m\(^{-3}K^{-1}\)) were determined from the intercept and slope, respectively, of the corresponding straight lines obtained from the evolution of density with temperature. Table 3 shows the density equation parameters, standard deviations (\(\sigma\)) and correlation factors (Adj. R\(^2\)) for the investigated temperature ranges for DESs. It can be noticed that the citric acid:glucose eutectic mixture has higher density than citric acid:fructose eutectic mixture at the temperature range of 293.15-343.15 K, but the density of citric acid:glucose DES declines rapidly after 353.15 K.

### Table 3. Constants of the density equation with standard deviations (\(\sigma\)), correlation factors (Adj. R\(^2\)) and temperature ranges for (1:1 M) citric acid:glucose and citric acid:fructose DESs

<table>
<thead>
<tr>
<th>DES</th>
<th>Temp. range (K)</th>
<th>Coefficients of Eq. (2)</th>
<th>Adj. R(^2)</th>
</tr>
</thead>
<tbody>
<tr>
<td>DES1</td>
<td>293.15-363.15</td>
<td>a (kg·m(^{-3})) = 3194.30, (\sigma [a] = 6.4735), (b (kg·m^{-3}K^{-1}) = -4.9095), (\sigma [b] = 0.0213)</td>
<td>0.9966</td>
</tr>
<tr>
<td>DES2</td>
<td>293.15-363.15</td>
<td>a (kg·m(^{-3})) = 1912.50, (\sigma [a] = 0.7736), (b (kg·m^{-3}K^{-1}) = -1.2223), (\sigma [b] = 0.0022)</td>
<td>0.9992</td>
</tr>
</tbody>
</table>

For all systems, a very good linear correlation and behaviour was observed between density and temperature, like described for pure ionic liquids [22-24]. The density values for these DESs decline from 1748.38 to 1412.38 kg·m\(^{-3}\) (for citric acid:glucose) and from 1553.68 to 1467.00 kg·m\(^{-3}\) (for citric acid:fructose) for the temperature range of 293.15-363.15 K.

Hayyan et al. [25] studied choline chloride (2-hydroxyethyl-trimethylammonium)-based DESs with D-glucose in different molar ratios (1:1; 1.5:1; 2:1; 2.5:1; 1:1.5; 1:2; 1:2.5) and concluded that these DESs at different ratios were colourless even after heating at high temperature (358.15 K), which indicated that caramelization reactions did not occur at this temperature. All densities of ChCl-D-glucose DESs were above 1200.00 kg·m\(^{-3}\), and these values were between the room temperature densities of pure ChCl (1185.60 kg·m\(^{-3}\)) and that of pure D-glucose (1534.50 kg·m\(^{-3}\)). ChCl-D-glucose DES (molar ratio 1:1) had the density of 1297.80 kg·m\(^{-3}\) at room temperature and 1265.90 kg·m\(^{-3}\) at 358.15 K, but ChCl-D-glucose DES (molar ratio 2:1) had the density of 1211.50 kg·m\(^{-3}\) at 358.15 K. Compared to the reported physical properties of phosphonium-based DES by Kareem et al. [26] it was noted that ChCl-D-glucose DES (molar ratio 1:1) had similar values to the DES constituted from [methyltriphenylphosphonium bromide:glycerol] at the molar ratio of 1:1.75. ChCl-D-glucose DESs with molar ratios of 1.5:1; 2:1; and 2.5:1 had the densities close to the DES made from [methyltriphenylphosphonium bromide:glycerol] at the molar ratio of 1:4. ILs such as 1-hexyl-1-methyl-pyrrolidinium bis (trifluoromethylsulfonyl) imide had higher density (1340.00 kg·m\(^{-3}\) at 293.15 K) than ChCl-D-glucose DES (molar ratio 1:1) [27]. ChCl-D-glucose DESs in molar ratios 1.5:1; 2:1; 2.5:1 have similar densities as some imidazolium and pyrrolidinium based ILs, such as 1-ethyl-3-methylimidazolium methylsulfate and 1-butyl-1-methylpyrrolidinium trifluoromethanesulfonate, which have the density values of 1280.00 and 1298.15 kg·m\(^{-3}\) at 293.15 K, respectively [27]. It can be easily established that the glucose-based DESs have comparable densities that can be compared to other DESs and some common ILs.

Additionally, Hayyan et al. [28] measured the densities of ChCl-D-fructose DESs at different ratios (1:1; 1.5:1; 2:1; 2.5:1), and reported that the values were less than 1340.00 kg·m\(^{-3}\). The density of these ChCl-D-fructose DES increased with the increase of the ChCl molar ratio. ChCl-D-fructose DES with the molar ratio 1:1 had the density of 1337.00 kg·m\(^{-3}\) at room temperature and 1226.90 kg·m\(^{-3}\) at 358.15 K. ChCl-D-fructose DES with molar ratio 2.5:1 had the density of 1211.50 kg·m\(^{-3}\) at 358.15 K. ChCl-D-fructose DES (molar ratio 1:1) had approximately a similar density range to the DES made of [methyltriphenylphosphonium bromide:glycerol] at the ratio of 1:1.75. IL [1-butyl-1-methylpyrrolidinium trifluoromethanesulfonate] had the density 1200.00 kg·m\(^{-3}\), very close to the density of ChCl-D-fructose DES (molar ratio 2.5:1) at room temperature [26]. Ionic liquid [1-amyl-3-methylimidazolium hexafluorophosphate] had a high density (1320.00 kg·m\(^{-3}\)), close to ChCl-D-fructose DES (molar ratio 1:1) at room temperature [27]. However, ILs can have much higher density values, such as 2400.00 kg·m\(^{-3}\) reported for the IL [(CH\(_3\))\(_3\)S][Al\(_2\)Br\(_7\)] [29]. It can be said that the D-fructose based DESs have similar densities to other reported DESs and ILs.

The expansion with temperature is best quantified by the thermal expansion coefficient (\(\alpha\)), defined in equation (3) as:

\[ \alpha = -\frac{1}{\rho} \left( \frac{\partial \rho}{\partial T} \right) \]  

It can be obtained by the ln \(\rho - T\) plot, fitted according to the straight line from the equation (4):

\[ \ln \rho = c - \alpha \cdot T \]
The molecular volume \( V_m \) can be calculated by the equation (5):

\[
V_m = \frac{M}{N_A \cdot \rho}
\]  

where M is molar mass and \( N_A \) is Avogadro’s constant \((6.022 \cdot 10^{23} \text{ mol}^{-1})\). Also, the volume and density may be substituted for one another since they have the inverse mathematical relation (Eq. 6):

\[
V_m \left(\text{nm}^3\right) = \frac{M \left(\text{g} \cdot \text{mol}^{-1}\right)}{602.2 \cdot \rho \left(\text{g} \cdot \text{cm}^{-3}\right)}
\]  

where the factor 602.2 derives from the Avogadro constant. The values of molecular volume at 303.15 K were found to be 0.3768 nm\(^3\) for citric acid:glucose (1:1) and 0.4204 nm\(^3\) for citric acid:fructose (1:1). Many properties correlate rather closely with the formula unit volume. Glasser [30] listed linear correlations observed between the formula volume and heat capacity, entropy, and lattice energy. The heat capacity and entropy correlations appear to be linear in formula volume, because larger volumes imply greater freedom of motion of the species involved. The smaller the distance between charges, the larger the lattice energy. Lattice energy is proportional to \( V_m^{-1/3} \) (where the \(-1/3\) exponent is needed to convert volume to distance). The lattice energy \( (U_{pot}) \) was calculated according to the equation (7) [30-31]:

\[
U_{pot} = 1981.2 \cdot \left(\frac{\rho}{M}\right)^{1/3} + 103.8
\]  

The lattice energy for the studied DESs were found to be 32.5857 kJ\text{-mol}^{-1} for citric acid:glucose (1:1) and 31.4220 kJ\text{-mol}^{-1} for citric acid:fructose (1:1) at the same temperature (303.15 K). The obtained values for these DESs are lower than those of molten salts, namely, the fused CsI has the lowest lattice energy among the alkaline halides and the value is 613.00 kJ\text{-mol}^{-1} [32]. This is primarily the reason why these DESs can exist in a liquid state close to room temperature. Heat capacity \( (C_p) \) was calculated according to the equation (8) for ionic liquids [30-31]:

\[
C_p = 1037 \cdot V_{mol} + 45
\]  

The obtained \( C_p \) values at 303.15 K are 435.7390 J\text{-K}^{-1}\text{-mol}^{-1} and 480.9343 J\text{-K}^{-1} for citric acid:glucose (1:1) and citric acid:fructose (1:1), respectively.

### Table 4. Constants of the equation (4) for temperature dependence of thermal expansion coefficient, together with standard deviations (σ), correlation factors (Adj. R\(^2\)) and temperature ranges for (1:1 M) citric acid:glucose and citric acid:fructose deep eutectic mixtures

<table>
<thead>
<tr>
<th>DES</th>
<th>Temp. range</th>
<th>Coefficients of Eq. (4)</th>
<th>Adj. R(^2)</th>
</tr>
</thead>
<tbody>
<tr>
<td></td>
<td>T (K)</td>
<td>c (kg·m(^{-3})·K(^{-1}))</td>
<td>σ (c)</td>
</tr>
<tr>
<td>DES1</td>
<td>293.15-363.15</td>
<td>8.3851</td>
<td>44.02·10(^{-4})</td>
</tr>
<tr>
<td>DES2</td>
<td>293.15-363.15</td>
<td>7.5861</td>
<td>6.84·10(^{-4})</td>
</tr>
</tbody>
</table>

Effect of temperature on the dynamic viscosity of two citric acid-based deep eutectic solvents

Viscosity data is important for the industrial chemical process design, fluid flow systems and for selecting suitable applications. Viscosity data of DES can be helpful for the selection of optimum salt:hydrogen bond donor ratio, which can consequently save both material and energy. In general, at atmospheric pressure, the increase in temperature results in the increase of the average speed of the molecules in the liquid. This leads to a decrease in the average intermolecular forces and, consequently, reduces the fluid resistance to flow, termed as the viscosity. Basically, the viscosity of ILs is influenced by the strength of their van der Waals interactions, the hydrogen bonding ability, and the planarity of the molecular structure [33]. In their systematic study of the viscosity of ILs, Okoturo and Van der Noot [34] concluded that the temperature variation of viscosity of ILs follows the Arrhenius equation or Vogel-Tamman-Fulcher (VTF) equation.

![Figure 4. Temperature dependence of the dynamic viscosity of the studied eutectic mixtures: citric acid:glucose \( \square \) and citric acid:fructose \( \circ \).](image)
where \( \eta, E_\eta, R, \) and \( T \) are constant for the given liq-
uid, the activation energy for the viscous flow, the gas
constant and the absolute temperature, respectively.

Figure 4 shows dynamic viscosities (\( \eta \)) of synthesized
citric acid-based deep eutectic mixtures. As it has been
observed for the density, the citric acid:fructose eutectic
mixture has a notably lower dynamic viscosity than the
citric acid:glucose eutectic mixture. Viscosity (\( \eta, \text{Pa} \cdot \text{s} \)) is
given as a temperature (\( T, \text{K} \)) dependence as a polyno-
mial equation of the third degree (10):

\[
\eta = a + b \cdot T + c \cdot T^2 + d \cdot T^3
\]

By using Excel program (Microsoft Office), “a”, “b”, “c”
and “d” parameters were obtained. The dynamic viscosity-
values for these DESs vary from 0.0370 to 5.4730
Pa·s (for citric acid:glucose) and from 0.0368 to 2.7000
Pa·s (for citric acid:fructose) for the temperature range
of 293.15-363.15 K. It can be noticed that our systems
have higher viscosity values on lower temperatures, but
drop rapidly during heating.

Few studies reported the viscosity of ILs [10] and, in
addition, DES physical properties data are even more
lacking. DESs that are liquid at room temperature are
both easy to handle and can be applied in many indus-
trial routes [26]. DESs that have high viscosity are not a
good choice for certain applications, like a liquid-liquid
extraction. Also, viscous solvents need to be preheated
before processing and require more pumping energy
[35]. Hayyan et al. [25] reported that, at room temper-
ature ChCl-D-glucose DES (molar ratio 2.5:1) had the
highest viscosity value of 10.9100 Pa·s, followed by ChCl-
D-fructose DES with the molar ratio of 10.4371 Pa·s. At 358.15, K ChCl-D-fructose DESs in different
molar ratios (1:1; 1.5:1; 2:1; 2.5:1) had the viscosi-
 ties of 0.2093, 0.1307, 0.0720, and 0.1083 Pa·s,
respectively. At 298.15 K these DESs had the viscosi-
ties of 9.0371, 8.0000, 8.0451 and 10.9100 Pa·s, re-
spectively. D-glucose-based DESs are more viscous
than some phosphonium-based DESs, especially at low
temperatures. According to Kareem et al. [26], at 338.15 K,
the viscosity value of 0.0166 Pa·s was reported for
[methyltriphenylphosphonium bromide:glycerol] DES
in the ratio of 1:1.75, and 0.0504 Pa·s for [methyltriph-
enylphosphonium bromide:ethylene glycol] DES in the
ratio of 1:4. In their study with ChCl-based DESs with
D-fructose in different molar ratios (1:1; 1.5:1; 2:1; 2.5:1),
Hayyan et al. [28] noted that at room temperature ChCl-
based DESs with D-fructose (molar ratio 2.5:1) had the
highest viscosity of 17.6455 Pa·s, followed by ChCl-
D-fructose DES with the molar ratio of 1.5:1 (14.3474
Pa·s). At 358.15, K ChCl-D-fructose DESs in different
molar ratios (1:1; 1.5:1; 2:1; 2.5:1) had the viscosities in
the range of 0.1293-0.2806 Pa·s. The lowest viscosity
at room temperature and at high temperature was re-
ported for ChCl-D-fructose DES with molar ratio of 2:1.
The authors recommended that, in order to reduce their
viscosity, D-fructose based DESs need to be heated to
higher temperatures, such as 318.15-328.15 K or even
to 338.15 K. D-fructose based DESs are much viscous
than other phosphonium-based DESs reported by other
studies [26].

If it is assumed that the fluid flow obeys the Arrhe-
nius equation [36-37], the temperature dependence of
liquid viscosity can also be expressed exponentially, as
in equation (11):

\[
\eta = \frac{E_\eta}{R \cdot T} e^{\frac{A_\eta}{R \cdot T}}
\]

where \( A_\eta \) is the pre-exponential factor, \( E_\eta \) is the activa-
tion energy for viscosity, \( T \) is absolute temperature (K),
and \( R \) is the universal gas constant (8.314 J·K\(^{-1}\)·mol\(^{-1}\)).
The pre-exponential factor, \( A_\eta \), is the frequency factor
and describes molecular collisions in the collision theory
and the entropy term in the transition state theory.
The activation energy \( E_\eta \) is an energy barrier that must be
overcome before the elementary flow process can occur.
Table 5 presents these equations for dynamic viscosities
of both studied DESs.

Table 5. Polynomial and exponential viscosity equations together with temperature ranges and
correlation factors for (1:1 M) citric acid:glucose and citric acid:fructose deep eutectic mixtures

<table>
<thead>
<tr>
<th>DES</th>
<th>Temp. range</th>
<th>Viscosity equation</th>
<th>Adj, R^2</th>
</tr>
</thead>
<tbody>
<tr>
<td></td>
<td>T (K)</td>
<td>( \eta ) (Pa·s)</td>
<td></td>
</tr>
<tr>
<td>DES1</td>
<td>293.15-363.15</td>
<td>( \eta = 9 \cdot 10^{-5} \cdot T^3 + 0.0104 \cdot T^2 - 4.0100 \cdot T + 513.65 )</td>
<td>0.9880</td>
</tr>
<tr>
<td></td>
<td></td>
<td>( \eta = 2 \cdot 10^{-5} \cdot e^{222.81/\sqrt{T}} )</td>
<td>0.9008</td>
</tr>
<tr>
<td>DES2</td>
<td>293.15-363.15</td>
<td>( \eta = 2 \cdot 10^{-5} \cdot T^3 + 0.0251 \cdot T^2 - 8.5833 \cdot T + 978.02 )</td>
<td>0.9944</td>
</tr>
<tr>
<td></td>
<td></td>
<td>( \eta = 3 \cdot 10^{-5} \cdot e^{93.42/\sqrt{T}} )</td>
<td>0.9199</td>
</tr>
</tbody>
</table>
The logarithmic form of the Arrhenius equation can also be used in order to describe the temperature dependence of viscosity, presented as in equations (12) and (13):

\[
\log \eta = \log A_\eta + \frac{E_\eta}{2.303 \cdot R \cdot T} \tag{12}
\]

or

\[
\ln \eta = \ln \eta_0 + \frac{E_\eta}{R \cdot T} \tag{13}
\]

It is obvious that the \( \log \eta \) or \( \ln \eta \) must also be a linear function of the reciprocal of the absolute temperature \((1/T)\). From the slope and intercept of the straight line, \( A_\eta \) and \( E_\eta \) can be calculated. The viscosity-temperature dependence can be fitted by the Arrhenius equation with high precision for studied deep eutectic mixtures, as shown in Table 6.

### Table 6. Arrhenius equations for viscosity with calculated pre-exponential factors and activation energies for DESs

<table>
<thead>
<tr>
<th>DES</th>
<th>Temp. range</th>
<th>Viscosity Arrhenius Equations</th>
<th>( A_\eta ) (Pa s)</th>
<th>( E_\eta ) (J·mol⁻¹)</th>
<th>Adj. R²</th>
</tr>
</thead>
<tbody>
<tr>
<td>DES1</td>
<td>293.15-363.15</td>
<td>( \ln \eta = 7222.8 \cdot (1/T) - 22.542 )</td>
<td>1.6223·10⁻⁰⁻⁰</td>
<td>60050.36</td>
<td>0.9406</td>
</tr>
<tr>
<td>DES2</td>
<td>293.15-363.15</td>
<td>( \ln \eta = 6634.2 \cdot (1/T) - 21.884 )</td>
<td>3.1326·10⁻⁰⁻⁰</td>
<td>55156.74</td>
<td>0.9523</td>
</tr>
</tbody>
</table>

As expected, \( E_\eta \) values for eutectic mixtures tested are larger than those for conventional liquids or high temperature molten salts [36-37], which can be explained by large ion to the hole radius ratio in these eutectic mixtures. The difference observed between the two DESs studied must arise from a better ability of monosaccharides to form hydrogen bonds through their chemical groups, which may explain differences in density and viscosity. It was previously stated by other authors [38] that alkyl chain lengthening or fluorination of organic components causes the increase in van der Waals interactions and hydrogen bonds, which makes ionic liquids be more viscous. Since high viscosity at low temperatures can negatively affect any technological process, it is recommended to use these DESs at the temperature not lower than 323.15 K.

### Figure 5. Temperature dependence of the conductivity of the studied eutectic mixtures: citric acid:glucose \( \square \) and citric acid:fructose \( \circ \).

Effect of temperature on the electrical conductivity of two citric acid-based deep eutectic solvents

The electrical conductivity of an IL (\( \kappa \)) is very important if it is considered to be a supporting electrolyte in electrochemical devices. The higher conductivity exhibited the lower ohmic drop during electrolysis and lower cell voltage, resulting in higher energy efficiency. For ILs the temperature-electrical conductivity dependence is described by the Arrhenius-type equation (14) [33]:

\[
\kappa = \kappa_\infty \cdot \exp \left[ -\frac{E_{\kappa,k}}{k_B \cdot T} \right] \tag{14}
\]

where \( \kappa_\infty \), \( E_{\kappa,k} \), \( k_B \), and \( T \) are electrical conductivity at infinite temperature, activation energy (energy needed for an ion to hop in a free hole), the Boltzmann constant, and absolute temperature, respectively. On the other hand, the conduction behaviour of most of the ILs does not follow the exponential dependence with the inverse of the temperature. The observed conductivity vs. temperature relationship can be described by VTF-type equation (15):

\[
\kappa = \kappa_\infty \cdot \exp \left[ -\frac{E_{\kappa,k}}{k_B \cdot (T - T_g)} \right] \tag{15}
\]

where \( T_g \) stands for the glass transition temperature. The equation can be also written as (16):

\[
\kappa = \kappa_0 \cdot \exp \left[ -\frac{B'}{(T - T_0)} \right] \tag{16}
\]

where \( \kappa_0 \), \( B' \), and \( T_0 \) represent the VTF fitting parameters. The plots of electrical conductivity values for the two deep eutectic mixtures as a function of temperature over the temperature range of 303.15-363.15 K are shown in Figure 5. The values of electrical conductivity increase with temperature for both investigated eutectic mixtures in the range of 0.00421-0.03090 S·m⁻¹ for eutectic mixture citric acid:glucose (1:1) and in the range of 0.25500-0.63300 S·m⁻¹ for eutectic mixture citric acid:fructose (1:1).
The figure clearly shows that the change in the electrical conductivity of eutectic mixture citric acid:fructose (1:1) is significant, while in the case of eutectic mixture citric acid:glucose (1:1) electrical conductivity changes very little with temperature.

Polynomial equations of second degree (17) expressing the temperature dependence of electrical conductivity (κ, S∙m⁻¹) is shown as:

\[ \kappa = a + b \cdot T + c \cdot T^2 \] ..........................(17)

where T represents the temperature (K). Also, the temperature dependence of electrical conductivity can also be expressed exponentially by using the Arrhenius equation (18):

\[ \kappa = A_\kappa \cdot e \frac{E_\kappa}{R \cdot T} \] ..........................(18)

where: Aκ represents the pre-exponential coefficient, Eκ represents the activation energy for electrical conduction, T represents absolute temperature (K), and R represents the universal gas constant (8.314 J∙K⁻¹·mol⁻¹). These equations for electrical conductivity of both studied ionic liquids are presented in Table 7. As previously done with viscosity data, the electrical conductivity of deep eutectic mixtures can also be fitted using the logarithmic form of Arrhenius equation (equations (19-20)) [39-40]:

\[ \log \kappa = \log A_\kappa - \frac{E_\kappa}{2.303 \cdot R \cdot T} \] ..........................(19)
or

\[ \ln \kappa = \ln \kappa_0 - \frac{E_\kappa}{R \cdot T} \] ..........................(20)

Table 7. Polynomial and exponential conductivity equations together with the temperature ranges and correlation factors for DESs (1:1 M) citric acid:glucose and citric acid:fructose

<table>
<thead>
<tr>
<th>DES</th>
<th>Temp. range</th>
<th>Conductivity equations</th>
<th>Adj. R²</th>
</tr>
</thead>
<tbody>
<tr>
<td>DES1</td>
<td>303.15-363.15</td>
<td>( \kappa = 2 \cdot 10^{-4} \cdot T^2 - 0.009 \cdot T + 0.1002 )</td>
<td>0.9954</td>
</tr>
<tr>
<td></td>
<td></td>
<td>( \kappa = 629.460 \cdot e^{-35671/T} )</td>
<td>0.9576</td>
</tr>
<tr>
<td>DES2</td>
<td>303.15-363.15</td>
<td>( \kappa = 2 \cdot 10^{-4} \cdot T^2 + 0.0368 \cdot T - 6.6854 )</td>
<td>0.9698</td>
</tr>
<tr>
<td></td>
<td></td>
<td>( \kappa = 58.983 \cdot e^{-5221/T} )</td>
<td>0.8900</td>
</tr>
</tbody>
</table>

Table 8. Arrhenius equations for conductivity with calculated pre-exponential factors and activation energies for DESs

<table>
<thead>
<tr>
<th>DES</th>
<th>Temp. range</th>
<th>Electrical Conductivity</th>
<th>( A_\kappa )</th>
<th>( E_\kappa )</th>
<th>Adj. R²</th>
</tr>
</thead>
<tbody>
<tr>
<td>DES1</td>
<td>303.15-363.15</td>
<td>In ( \kappa = -3567.3 \cdot 1/T + 6.4449 )</td>
<td>629.4837</td>
<td>29658.53</td>
<td>0.9743</td>
</tr>
<tr>
<td>DES2</td>
<td>303.15-363.15</td>
<td>In ( \kappa = -1622.3 \cdot 1/T + 4.0773 )</td>
<td>58.9860</td>
<td>13487.80</td>
<td>0.9320</td>
</tr>
</tbody>
</table>

Thermodynamic functions of activation of two citric acid-based deep eutectic solvents

In order to understand the viscous flow better, Eyring’s transition state theory was used for calculating the thermodynamic functions of activation from the dynamic viscosity. For liquid mixtures, the expression (21) for the dynamic viscosity can be written as [41,42]:

\[ \eta = \left( \frac{h \cdot N_A}{V} \right) \cdot e^{\frac{\Delta G^*}{R \cdot T}} \] ...........................................(21)

where: h represents the Planck’s constant; NA represents Avogadro’s number; V represents the molar volume of the eutectic mixture (the ratio of the average molar mass and density of the eutectic mixture); \( \Delta G^* \) represents the molar Gibbs energy of activation for the viscous flow process. Combining the previous equation with equation (22):

\[ \Delta G^* = \Delta H^* - T \cdot \Delta S^* \] ...........................................(22)

yields the equation (23):

\[ \ln \left( \frac{\eta \cdot V}{h \cdot N_A} \right) = \left( \frac{\Delta H^*}{R \cdot T} \right) - \left( \frac{\Delta S^*}{R} \right) \] ...........................................(23)

From the experimental density and viscosity data, it is possible to calculate \( \ln \left( \eta \cdot V/h \cdot N_A \right) \) as a function of \( 1/T \) for each system (Figure 6). From slope and intercept of the straight lines, the enthalpy (\( \Delta H^* \)) and entropy (\( \Delta S^* \)) of activation of viscous flow were calculated. The \( \Delta H^* \) values were constant in the studied temperature range.
Figure 6. Plots of ln (\(\eta\cdot V/h\cdot N_A\)) against the inverse temperature of the studied eutectic mixtures: citric acid:glucose - □ and citric acid:fructose - ○.

Table 9. The thermodynamic functions of activation of viscous flow, \(\Delta H^*, \Delta S^*, \Delta G^*\), and coefficients of correlation for tested DESs at 303.15 K

<table>
<thead>
<tr>
<th>DES</th>
<th>Eyring’s Eq.</th>
<th>(\Delta H^*(\text{kJ} \cdot \text{mol}^{-1}))</th>
<th>(T \cdot \Delta S^*(\text{kJ} \cdot \text{mol}^{-1}))</th>
<th>(\Delta G^*(\text{kJ} \cdot \text{mol}^{-1}))</th>
<th>Adj. R²</th>
</tr>
</thead>
<tbody>
<tr>
<td>DES1</td>
<td>ln ((\eta \cdot V/h \cdot N_A) = 6892.7-1/T - 8.1950)</td>
<td>57.3060</td>
<td>20.6546</td>
<td>36.6513</td>
<td>0.9365</td>
</tr>
<tr>
<td>DES2</td>
<td>ln ((\eta \cdot V/h \cdot N_A) = 6548.2-1/T - 8.2401)</td>
<td>54.4417</td>
<td>20.7683</td>
<td>33.6735</td>
<td>0.9506</td>
</tr>
</tbody>
</table>

Table 9 contains obtained values of thermodynamic functions of activation at 303.15 K, together with the coefficients of correlation for the fits to equation (23). It can be seen that the magnitude of molar enthalpy of activation for viscous flow is higher than \(T \cdot \Delta S^*\) values. We can conclude that the energetic contribution, which corresponds to the molar enthalpy of activation for viscous flow, is more important than the entropic contribution terms to the molar Gibbs energy of activation for viscous flow values. For these two investigated systems, the interactional factor is predominant over structural for the viscous flow process.

Relationship between molar conductivity and viscosity

The relation between ionic conductivity and molar conductivity is given by the equation (24):

\[
\Lambda = \frac{\kappa \cdot M}{\rho}
\]  

(24)

where \(\Lambda\) is the molar conductivity, \(\kappa\) is the ionic conductivity, \(\rho\) is the density and \(M\) is the average molecular weight. The empirical VTF equation for the observed temperature dependences of molar conductivity (25) can be expressed as:

\[
\Lambda = \Lambda_0 \cdot \exp \left[ \frac{-B'}{(T-T_0)} \right]
\]  

(25)

where \(\Lambda_0\), \(B'\), and \(T_0\) represent the VTF fitting parameters [33]. The relation between mobility of ions and viscosity is given by Walden rule (\(\Lambda \cdot \eta = \text{const}\); \(\lambda\) is the equivalent conductivity). If the manner of dissociation of a solute constituting an electrolytic solution is not known, the molar conductivity rather than the equivalent conductivity is used. Interestingly enough, the original Walden rule finds a new lease on life in current studies of ionic liquids of the ambient temperature variety, where the Walden plot, in the form \(\log (\Lambda)\) versus \(\log (\eta^{-1})\) is being used as a classification diagram to distinguish "normal" ionic liquids from "poor" ionic liquids, on the one hand, and "superionic" liquids on the other hand [43]. The Walden rule is useful for organizing and classifying the ILs [44]. For molten salts and ionic liquids it was found that it is more appropriate to use the “fractional” Walden rule, shown as equations (26-27):

\[
\Lambda \cdot \eta^\alpha = C
\]  

(26)

or

\[
\log \Lambda = \log C + \alpha \cdot \log \eta^{-1}
\]  

(27)
In this equations C is a temperature dependent constant called the Walden product, and α is a positive constant smaller than 1, representing the slope of the line in the Walden plot, which reflects the decoupling of the ions. The parameter α expresses the difference of the activation energies of the ionic conductivity and viscosity \([43,45,46]\). The variation of \(\log \Lambda\) vs. \(\log \eta^{-1}\) is shown in Figure 7.

The fractional Walden rule, which implies that the Arrhenius activation energy for conductivity is lower than that for viscosity, finds a natural interpretation in terms of one of the ionic species being smaller than the other, hence capable of squeezing through smaller gaps in the condensed phase structure. All the studied DESs obey the fractional Walden rule very well and the values of the Walden slopes are all smaller than unity (see Table 10), indicating the presence of obvious ion associations in the investigated DESs.

From Figure 7, it is obvious that the curves of the studied DESs are under the ideal line \([46]\). To fix the position of the ideal dotted Walden line from corner to corner of a square diagram in Fig. 7, the data for dilute aqueous KCl solution \([47]\), comprising of equal mobilities of fully dissociated ions \([48]\), were used. Another way used for calculating the α is the ratio of the temperature-dependent activation energies for viscosity and molar conductivity \((\alpha = \frac{E_{\alpha,\Lambda}}{E_{\alpha,\eta}} < 1)\). These results mean that in the investigated DESs there are not only charge carrying species simply formed by citric acid, because if that was the case all slopes would have to be similar. In the case under discussion, it is likely that the conduction here involves some degree of cooperation of the ions concerned. Here lies a resemblance to the process of the viscous flow from molten salts, where due to the imposed condition of electroneutrality the translation of ions of both signs is involved. But because all the investigated DESs are under the ideal line, this shows that these ILs are also "subionic", and we believe that their special accumulation structure also account for this phenomenon.

### Table 10. Walden equation coefficients along with the standard deviations (σ), regression coefficients (Adj. R²) and the temperature ranges for the DESs

<table>
<thead>
<tr>
<th>DES</th>
<th>Temp. range (K)</th>
<th>Coefficients of Walden Eq.</th>
<th>Adj. R²</th>
</tr>
</thead>
<tbody>
<tr>
<td></td>
<td></td>
<td>α</td>
<td>σ [α]</td>
</tr>
<tr>
<td>DES1(^1)</td>
<td>303.15-363.15</td>
<td>0.4890</td>
<td>0.1130</td>
</tr>
<tr>
<td>DES2(^2)</td>
<td>303.15-363.15</td>
<td>0.2726</td>
<td>0.0156</td>
</tr>
</tbody>
</table>

\(^1\)log \(\Lambda = -5.6170 + 0.4690 \cdot \log \eta^{-1}\)

\(^2\)log \(\Lambda = -4.1668 + 0.2726 \cdot \log \eta^{-1}\)

The esterification of oleic acid in the presence of eutectic mixture citric acid: glucose (1:1) with the use of sulfuric acid as a catalyst.

Figure 8 presents the change in the conversion of oleic acid into the ethyl oleate \((X_A)\) with the use of catalyst sulfuric acid (1% relative to the weight of oleic acid), as function of reaction time. Neither DES1 nor DES2 proved to be catalysts when used solely in the reaction. Although the reaction has a better start when DESs are present in the reaction mixture, and DES2 gives a better conversion degree of oleic acid into ethyl oleate than DES1, clearly it is better when these DESs are excluded from the reaction mixture. We assume that the interaction of eutectic mixture with the reactants (oleic acid, ethyl alcohol and sulfuric acid) is low, but that the slowdown of the reaction in the presence of a eutectic mixture may be caused due to the increase in viscosity after the addition of the eutectic solvent.
The fractional walden rule was applied in establishing volume, lattice energy and heat capacity of these DESs. The viscosity and conductivity values of these DESs show viscosity of the systems decreases linearly with temperature, while the electrical conductivity increases. The relationship between the density, viscosity and conductivity is determined by the strength of the interactions present in the systems. In both cases of deep eutectic solvents, the density and viscosity values are similar to some ionic liquids. Since it is noticed that the studied DESs have high viscosity and density at room temperature, industrially it is recommended to heat up these DESs before processing. Despite the fact that these DESs were proven not to be good cosolvents in oleic acid ethanolation, the authors hope that the future application of these DESs will be found and successfully achieved.

Acknowledgements

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References

EUTEKTIČKI RASTVARAČI NA BAZI LIMUNSKE KISELINE: FIZIČKE OSOBINE I NJIHOVA UPOTREBA KAO KOSOLVENATA U ETANOLIZI OLEINSKE KISELINE KATALIZOVANE SUMPORNOM KISELINOM

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Eutektički rastvarači (DESs) su analozi „zelених” jonskih tečnosti (IL), i njihove mnoge povoljne osobine ih čine interesantnim za naučnu zajednicu. U ovom radu dva nova eutektička rastvarača na bazi limunske kiseline sa monosaharidima D-glukozom ili D-fruktozom (u molarnom odnosu 1:1) su pripremljene i okarakterisane. Na atmosferskom pritisku gustina, dinamički viskozitet i električna provodljivost ovih eutektičkih rastvarača su izmereni i analizirani kao funkcija temperature u praktičnom temperaturnom opsegu od 293.15-363.15 K. Arenijusova teorija je primenjena za razumevanje fenomena transporta u ovim eutektičkim rastvaračima. Korišćenjem eksperimentalnih podataka, izračunata su neka važna svojstva, kao što su, molekularna zapremina, energija rešetke, toplotni kapacitet, molarna Gibsova energija, entalpija i entropija aktivacije viskoznog protoka za sintetisane eutektičke rastvarače. Frakciono Valdenovo pravilo je korišćeno za određivanje odnosa između molarnih provodljivosti i viskoziteta, čime se pokazalo odlično linearno ponašanje.

Konačno, ovi eutektički rastvarači su testirani kao kosolventi u etanolizi oleinske kiseline. Sintetisani eutektički rastvarači poseduju mnoge poželjne osobine, poput niskog pritiska pare, nezapaljivost, biorazgradivost i mogu se dobiti iz raspoloživih obnovljivih izvora. Ovi eutektički rastvarači pokazuju potencijal za korišćenje u nekim industrijskim procesima, kao što su obrada i separacija hranljivih sastojaka, farmaceutski procesi i kao medijumi za hemijske reakcije.